

## TITLE OF THE INVENTION

METHOD FOR PROCESSING A PREFORM FOR OPTICAL FIBER,  
BURNER SYSTEM USEFUL FOR CARRYING OUT THE METHOD AND  
APPARATUS COMPRISING THE BURNER SYSTEM

5

## BACKGROUND OF THE INVENTION

## Field of The Invention

This invention relates to processing of a preform for optical fiber,  
10 and more particularly, to a method for processing an optical fiber preform by  
use of a specific type of burner system and to an apparatus suited to carry out  
the processing method. The invention also relates to a burner system which is  
adapted for use in the method and apparatus mentioned above.

## Related Art

15 For the manufacture of optical or lightguide fibers, a porous glass  
matrix is initially made by deposition of fine particles of glass by a  
vapor-phase axial deposition (VAD) technique, an outside vapor deposition  
technique (OVD) or the like. The glass matrix is dehydrated and sintered or  
consolidated to obtain a clear vitrified mother ingot. This ingot is then  
20 roughly drawn, in an electric furnace, into a primary processed product called  
preform whose diameter is reduced to an extent as adapted for use in fiber  
drawing.

The preform obtained in this manner is subsequently subjected to a  
secondary processing procedure using, for example a glass-working lathe.  
25 This secondary processing procedure includes an elongation procedure of  
adjusting an outer diameter in high precision, a flame polishing procedure  
wherein silica powder (hereinafter referred to as silica cloud) deposited on the

surface of the preform and fine defects are removed, with the attendant removal of a thermal stress left inside the preform, a drawing procedure where the preform is processed into a shape suited for fiber drawing at an end thereof, and the like.

5           The outer diameter of the preform should be precisely adjusted.

With a preform whose outer diameter is not uniform, when such a preform is set in a heating furnace of a fiber drawing apparatus and started to feed in, a space is inevitably established between a gas sealing member of the heating furnace and the preform. As a result, many problems would arise in that the probability of fiber breakage increases owing to the oxidation of furnace materials, deposition of foreign matters and the like and the variation in fiber diameter increases due to a gas flow being changed inside the heat furnace. For these reasons, the variation of the outer diameter should be usually suppressed to a level of below  $\pm 1\%$  along the length of the preform.

15           The silica cloud deposited on the preform surfaces and defects in the surfaces may lead to an abrupt variation of fiber diameter and may result, in the worst case, in the breakage of the preform. Thus, it is desirable to remove the cloud and defects by subjecting the preform to flame polishing at a processing stage thereof.

20           For shortening the time of from the commencement of fiber drawing of a preform to the stabilization in diameter of an optical fiber, it is favorable to process the preform, particularly at the end or ends thereof, in a tapered form as is particularly shown in Fig. 6.

As having set forth hereinabove, the processing of a preform may be divided into several different procedures, for which appropriate heating power and flame shape or thickness that depend on the respective procedures are required for easy and reliable control of the respective processing

procedures.

For a conventional burner unit used for preform processing, a small-sized, compact burner made of silica glass or a stainless steel and having such a structure as shown in Fig. 7 is employed. In practice, four to  
5 six small-sized burners (e.g. four burners B1 to B4 in Fig. 8) are arranged as shown in Fig. 8 to provide a burner unit U. Alternatively, a number of the burners of the type shown in the figure have been in use as arranged in a semi-circular or circular form.

These burners are each supplied with a supporting gas and a  
10 flammable gas therein. The combustion flame of a gas mixed at the inside or outlet of the burner is used to heat a preform for desired processing purposes. In general, oxygen is used for the supporting gas and hydrogen or methane or propane is used for the flammable gas. In this art, the type of burner is broadly classified into a premixing type gas burner wherein gases are  
15 premixed inside the burner beforehand and burnt at the tip of the burner and a post-mixing type gas burner wherein gases are separately fed to the pipe of the burner, and mixing and combustion are allowed to occur simultaneously at the tip of the burner.

When using hydrogen as a flammable gas, backfire is liable to occur  
20 wherein hydrogen burns inside the burner. In this sense, choice of the latter is preferred. This type of burner is described, for example, in Japanese Laid-open Patent Application No. 52-45740.

Another instance of a burner used for processing a preform is described, for example, in Japanese Laid-open Patent Application No.  
25 2000-220810 wherein a number of nozzles for supporting gas are arranged in a specific manner. More particularly, a number of inner pipes through which a supporting gas is passed are accommodated in an outer cylinder, into which

a flammable gas is fed, at different intervals depending on the location inside the outer cylinder. That is, the inner pipes are located more densely at a position nearer to the outer periphery of the cylinder. In this burner, a supporting gas and a flammable gas are mixed at the tip of the burner  
5 thereby obtaining a flame of potential heat power thereat.

In conventional burners, the thickness and intensity of a gas flame have been changed by changing the flow rates of a supporting gas and a flammable gas, respectively.

When a preform is processed by use of such a burner under  
10 conditions where a flame is turned down, for example, the flow rates of gases are made small, so that the heating power becomes weakened. More particularly, it has been difficult to obtain high heating power under thin flame conditions.

Accordingly, with the case where a thin, intense flame is required,  
15 e.g. when a preform is tapered at an end thereof in a manner as shown in Fig. 6, it is necessary to heat a limited narrow region alone so that the diameter of the preform is made small. In contrast, when a preform is heated by means of a thick flame, the preform is heated over a wide region thereof, making it difficult to form a well-tapered end.

20 Of course, when the flame is turned up and made thick and the heating region is extended, the flow rates of gases increase, so that heating power becomes high. This makes it difficult to obtain a weak gas flame. In the drawing and flame polishing procedures of adjusting an outer diameter, gentle heating over a wide range of a preform is necessary. If a flame is  
25 made thick, heating power has become too intense to process the preform in high precision. For the burner used in such a situation as set out above, it is desirable that the thickness of a gas flame can be adjusted arbitrarily

depending on the diameter of a preform and that the heating power of the flame can also be arbitrarily controlled depending on the conditions being applied to the preform.

5 A flame controlling method of minimizing a residual strain by flame polishing is described, for example, in Japanese Laid-open Patent Application No. 256027.

In Japanese Laid-open Patent Application Nos. 2000-143268 and 2000-203864, a preform end drawing method and an apparatus for carrying out the method are described. However, any method of controlling a burner  
10 flame over a wide range covering different preform processing procedures is not described at all.

As having stated hereinbefore, for processing of a preform, it is desirable to make a flame whose thickness and intensity can be changed over a wide range depending on the processing procedure and conditions. With  
15 conventional burners, it is extremely difficult to form different types of flames, including thin and thick, intense and weak flames, from the same burner that depend on the processing procedures and conditions.

#### SUMMARY OF THE INVENTION

It is accordingly an object of the invention to provide a method for  
20 automatically processing a preform, by use of one burner unit, in different ways including dummy bonding, elongation, flame polishing, drawing of the preform at an end or ends thereof, flame cutting and the like.

It is another object of the invention to provide a burner system,  
which is particularly suitable for realizing the method and apparatus of the  
25 invention.

It is a further object of the invention to provide an apparatus suited to carry out the method mentioned above and comprising the burner system

mentioned above.

The above objects can be achieved, according to one embodiment of the invention, by a method for processing a preform supported with a stationary chuck and a movable chuck of a glass-working lathe, which method comprising providing a burner of a type which is able to create flame-controlled conditions by controlling flow rates of a flammable gas and a supporting gas wherein the supporting gas is discharged from at least one group of discharge pipes co-axially classified into plural groups that are, respectively, controllable with respect to a gas flow rate, and processing a preform under the flame-controlled conditions.

Preferably, the plural groups of the discharge pipes are provided within a hollow body through which the flammable gas is passed, and the plural groups are co-axially arranged within the hollow body from a center of the hollow body toward an outer periphery, and the discharge pipes are so arranged that the supporting gas is passed therethrough in a manner as to be controllable in every group.

The hollow body is preferably a hollow cylinder and the plural groups of discharge pipes which are concentrically disposed within the hollow cylinder closed at one end and opened at the other end.

According to another embodiment of the invention, there is provided a burner system which comprises: a structure including a hollow body closed at one end and opened at the other end, through which a flammable gas is passed, and plural groups of coaxially arranged inner discharge pipes, accommodated in the hollow body, through which a supporting gas is passed; gas feed lines connected to the hollow body and the plural groups at one ends of the gas feed lines, respectively; and gas sources connected to the hollow body and the plural groups through the gas feed lines at the other ends

thereof, respectively, wherein each gas feed line has a control means for controlling a flow rate of a gas to be passed therethrough.

Preferably, the hollow body is a hollow cylinder and the plural groups of the inner discharge pipes are concentrically arranged within the hollow cylinder, respectively. More particularly, the inner discharge pipes are classified into groups in a concentric fashion.

According to a further embodiment of the invention, there is also provided a processing apparatus including the burner system defined above.

#### BRIEF DESCRIPTION OF THE ACCOMPANYING DRAWINGS

Fig. 1 is a schematic side view of a glass-working lathe according to the invention;

Fig. 2 is a schematic perspective view showing an instance of a burner unit according to the invention;

Figs. 3A and 3B are, respectively, a top view showing a nozzle portion of the burner shown in Fig. 2 wherein Fig. 3A shows inner nozzles grouped in three or four sections and Fig. 3B shows a modification of a nozzle arrangement in an innermost section;

Fig. 4A is a schematic view showing an instance of gas pipes for controlling gas flow rates through control valves or means according to the invention and Fig 4B is a schematic view showing a distributor structure for the respective gases;

Figs. 5A to 5E are, respectively, different processing procedures of a preform to which a burner unit according to the invention is applied;

Fig. 6 is a schematic view illustrating an ideal shape of an end of a preform for subsequent fiber drawing;

Fig. 7 is a schematic sectional view showing a conventional compact burner; and

Fig. 8 is a perspective view showing an instance of a conventional burner arrangement including four compact burners having such a structure as illustrated in Fig. 7.

## EMBODIMENTS OF THE INVENTION

5 Preferred embodiments of the invention are described in detail with reference to the accompanying drawings, particularly Figs. 1 to 5A to 5E. It will be noted that like reference numerals indicate like parts or members throughout the specification.

Fig. 1 shows, in a simplified form, a typical arrangement of a  
10 glass-working lathe useful for processing a preform according to the invention. A glass-working lathe GL is shown as including a preform 10 which is rotatably held with stationary and movable chucks 12, 14 at opposite ends thereof. The chuck 12 is supported with a stationary support 16 and the movable chuck 14 is supported with a tailstock 18 for pulling or pushing the  
15 preform 10 as shown in the figure in such a way that the preform is kept horizontally. These supports 14, 16 are, in turn, mounted on a base 20. A burner 22 is mounted on a carriage 24 that is associated with a displacement means 26, such as a screw, for displacing the carriage 24 longitudinally. The displacement means 26 is so set as to be parallel to an axis connecting the  
20 chucks 12, 14 and is driven with a motor 28 through a chain 29, a gear (not shown) and the like. The tailstock 18 is likewise driven with a driving unit (not shown).

The burner 22 is connected to gas sources 30, 31 through lines 30 and 32. The line 30 has branch lines 30a, 30b, 30c which are, respectively,  
25 connected to the burner 22 through valves 34a, 34b, 34c and mass flow controllers 36a, 36b, 36c. On the other hand, the line 32 is likewise connected to the burner 22 through a valve 34d and a mass flow controller



36d. The valves 34a to 34d and the mass flow controller 36a to 36d are, respectively, controlled by means of a control unit described hereinafter. In the practice of the invention, a burner system is constituted of the burner 22, the lines 30, 32 including branch lines 30a, 30b, 30c, and a flow rate control means including the valves 34a to 34d and the mass flow controllers 36a to 36d. The respective control means may be made of any other means such a control valve connected to the control unit so far as the flow rate of a gas can be controlled. It will be noted that the term "preform" is intended to mean not only a preform having a diameter of 20 to 100 mm, but also a silica glass matrix having a diameter of 100 mm or below.

In Fig. 1, the preform is kept horizontally, and may be kept in a vertical fashion as is known in the art.

In operation, while moving longitudinally the tailstock 18 under computer-controlled conditions toward the right side as viewed in the figure and indicated by arrow A, the burner is moved, for example, along a direction opposite to the tailstock 18 as indicated by arrow B, or may be stopped or moved in the same direction as the tailstock 18. In other words, the burner 22 is arranged to arbitrarily move in opposite directions. The preform 10 is applied with heating power from the burner 22, which varies depending on the type of processing. According to the invention, different processing procedures of a preform including dummy bonding, elongation to a predetermined value of an outer diameter, flame polishing, drawing of a preform to provide a well-shaped form suited for fiber drawing, flame cutting and the like are realized using a specific type of burner system that has such a structure as to arbitrarily control the degree of heating power in every gas flow line for a supporting gas irrespective of the thickness of a burner flame.

Reference is now made to Figs. 2 to 4 wherein the burner 22 useful

for carrying out the processing method of the invention is illustrated. As shown in Fig. 2, the burner 22 includes an outer hollow cylinder 40 with a hollow truncated cone-shaped form at an upper portion thereof for allowing a flame to be converged, and a plurality of inner pipes 42 through which a supporting gas is discharged. Reference numeral 44 indicates spaces other than the inner pipes 42 within the outer hollow cylinder 40, from which a flammable gas is discharged and mixed with the supporting gas from the inner pipes 42 at the burner port.

The plurality of inner pipes 42 are classified into three groups in Fig. 3A. More particularly, the inner pipes 42 are classified as accommodated in three concentric sections S1, S2 and S3 within the outer hollow cylinder 40 as viewed from above. The section S1 indicates a region between concentric circular lines C1 and C2, the section S2 is for a region between concentric circular lines C2 and C3, and the section S3 is within a region indicated by a circular line C3. In practice, no circular lines C1, C2 and C3 exist but are depicted only for convenience's sake. The inner pipes 42 in each section are taken as one group and the groups of the inner pipes 42 are separately controlled with respect to the gas flow rate. As a matter of course, the number of the sections or groups may be 3 or more. For instance, the outer hollow cylinder may be concentrically divided into four sections wherein the section S2 is further divided into halves in a manner as indicated by a dotted line C4 between the circular lines C2 and C3.

With respect to the innermost section, at least one inner pipe 42 is depicted in Fig. 3A. The inner pipes 42 are usually accommodated, as shown in Fig. 3A, in such a way as to be more dense from the center of the outer cylinder toward the outer periphery thereof although up to three inner pipes may be set at the innermost section S3 as shown in Fig. 3B.

The outer hollow cylinder 22 is closed at the bottom thereof and has an inlet for a flammable gas and plural inlets for a supporting gas as will be hereinafter described in more detail with reference to Figs. 4A and 4B. The inner pipes 42 provided at the sections S1, S2 and S3 are, respectively,  
5 connected to the inlets of the outer hollow cylinder 22.

The outer hollow cylinder 22 has been illustrated hereinabove. Hollow bodies having different shapes such as a rectangle, polygons and the like may also be used in place of the hollow cylinder. In this case, inner pipes are arranged along the profile or outer shape of the hollow body  
10 wherein groups of the inner pipes may be arranged in similar forms of the outer shape of the hollow body. Preferably, the inner pipes are located more densely from the center toward the outer side. The hollow body is preferably cylindrical.

In this arrangement, a flammable gas such as hydrogen, methane,  
15 propane or the like is passed through the hollow outer cylinder 40, and a supporting gas such as of oxygen is passed through the inner pipes 42. Thus, the supporting gas and the flammable gas are separately fed into the burner 22 and mixed at the tip or burner port thereof and combusted.

For the control of the gas flow rates passing through the inner pipes  
20 42 and the spaces 44 in the respective sections S1 to S3, the line 30 connected to a supporting gas source 31 is trifurcated as the branch lines 30a, 30b, 30c which are, respectively, connected to joints 50a, 50b, 50c for supplying the gas to the outer hollow cylinder 22 through a distributor structure D. A line 32 for a flammable gas is connected to a joint 50d attached to the side wall of  
25 the outer hollow cylinder 22. Each line has a hand valve indicated at 34a, 34b, 34c or 34d and a mass flow controller (which may be hereinafter sometimes referred to as MFC) indicated at 36a, 36b, 36c or 36d, with which

gas flow rates can be, respectively, controlled with a signal outputted from a control unit C through lines 52a, 52b, 52c, 52d as shown. This type of control unit is known in the art and is not described in detail herein.

5 The reason why the hand valve 34a, 34b, 34c or 34d and the mass flow controller indicated at 36a, 36b, 36c or 36d are provided is as follows. When a preform is processed while an operator manually controls the respective flow rates, the MFC's are all fully opened, under which the valves are manually operated to change the flow rates as desired. On the other hand, where the flow rates of gases are automatically controlled such as by a  
10 computer in the control unit C, the valves are fully opened so that the flow rates are, respectively, controlled by means of the mass flow controllers. Of course, control valves or other control means may be used in place of the combination of a hand valve and a mass flow controller as is well known in the art.

15 The distributor structure D is described. This is particularly depicted in Fig. 4B. The distributor structure D of Fig. 4B is arranged as follows: the joint 50b is directly connected to the inner pipe 42 in the section or region S3; the supporting gas passed through the joint 50c is transmitted to a group of inner pipes 42 in the section S2; the supporting gas supplied through the  
20 joint 50a is passed to a group of inner pipes 42 in the section S1; and the flammable gas passed through the joint 50d is distributed throughout the outer hollow cylinder other than the inner pipes. Reference numerals 60, 62, respectively, indicate a partition plate for ensuring hermetic, complete separation of the gases from the respective joints.

25 The burner system is operated in the following manner. When a flammable gas from the gas source 33 is passed to the outer cylinder 40 through the line 32, MFC 36d, valve 34d, and joint 50d. On the other hand,

a supporting gas is passed and distributed to the respective groups of inner pipes 42 through the corresponding MFC's, hand valves, and joints.

In the burner structure as set forth hereinabove, the supporting gas runs through at the outer region S1 (i.e. closer to the outer periphery) in amounts larger than at the inner region (closer to the center region S3),  
5 whereas the flammable gas flows out in amounts larger at a portion closer to the central axis of the outer cylinder. Both gases are mixed at the port of the burner and combusted as 56 in Fig. 4A.

Since the supporting gas runs off in larger amounts at the outer  
10 peripheral section as 1, the flame 56, shown in Fig. 4A, is not extended beyond the opening of the outer cylinder. This allows flow rates of the flammable gas and the supporting gas in each section to be readily controlled. Thus, easy control of the shape or thickness of the flame, heating region, the distribution of temperature that depend on the type of preform processing  
15 procedure is ensured.

If the number of groups of the inner pipes within the outer hollow cylinder of the burner is increased, the intensity of a flame may be more precisely controlled, but with the control being more complicated. In the practice of the invention, it is preferred to provide three or four sections or  
20 groups of inner pipes as is shown in Fig. 3.

Metals such as stainless steels, silica glass and the like may be mentioned as a material for the burner. In view of the high reproducibility and the ease in increasing the number of inner fine pipes, a metal is preferred except the case where high cleanliness is required. If high  
25 cleanliness is necessary, silica glass is favorably used.

For carrying out several different preform processing procedures, the inner diameter of the outer cylinder generally ranges from 25 to 50 mm, and

an opening diameter of the inner pipe generally ranges from 1 to 3 mm.

These diameters may vary depending on the manner and the number of inner pipes arranged in each section. The flow rate of a flammable gas supplied from a gas source is generally set at a value within a range of up to 500 SLM (standard liter per minute), and the flow rate of a supporting gas is set at a value within a range of 0 to 300 SLM. In this connection, however, the inner pipe diameter may be varied depending on the section and the type of processing.

In the present invention, the inner pipes are arranged in plural sections in a manner as being controlled in individual sections with respect to the flow rate. If necessary, a gas flow in a given section may be stopped by closing a corresponding hand valve. As will be apparent from the foregoing, the flow rates of both a flammable gas and a supporting gas can be arbitrarily controlled wherein the flow rates of the supporting gas in different regions or sections, cylindrically separated, for example, of the outer hollow cylinder as viewed from above can be, respectively, controlled. Thus, a very precise control of a flame with respect to the thickness and intensity becomes possible with ease. Easy control of a flame leads to easy control of processing procedures. More particularly, parameters essentially required for processing of a preform include the intensity and thickness of a flame, i.e. an oxyhydrogen flame in this case, and the movements and moving speeds of the burner and tailstock. These parameters are interrelated with one another, and conventional preform processing procedures have been carried out under relatively rough control in the intensity and thickness of a flame in relation to other parameters. As a matter of course, a more precise control of the flame leads to a more reliable, easier control of many preform processing procedures without adjustment of a distance between the preform and a

burner port and without change of a burner unit with another type of burner unit for permitting a more precise control of a flame for a selected processing procedure. This leads to saving of time and labor undesirably required for the adjustment and the change. More particularly, if a flame is not precisely,  
5 reliably controlled, it undesirably becomes necessary to change the distance between a burner and a preform suited for every cycle of processing procedure and to replace a burner per se with a more appropriate one. This problem can be overcome by use of the burner system according to the invention wherein flame conditions can be appropriately controlled by  
10 controlling flow rates of a flammable gas and a supporting gas. The precise flame control can be realized by controlling the flow rates of a supporting gas passed through plural groups of inner pipes, which are concentrically separated from one another, for example.

The processing procedures of a preform using the burner system  
15 according to the invention are particularly described with reference to Figs. 5A to 5E.

Fig. 5A schematically shows dummy bonding including a heating step and a bonding-by-press step. In the figure, a dummy rod 70 having a cone-shaped tip portion 72 and used to hold a preform 10 is heated for  
20 bonding with the preform 10 while moving a tailstock along the direction indicated by the arrow without moving the burner to such an extent that part of the preform is molten. This procedure requires the most intense heating power. For example, when using a preform having a diameter of 60 mmφ and a burner of the type shown in Fig. 3A, flow rates of hydrogen used as a  
25 flammable gas and oxygen supplied to inner pipes at S1, S2 and S3 are as shown in Table 1 below.

Table 1

Flow rate of hydrogen (SLM)	Flow rate of oxygen		
	Group of inner pipes in S1	Group if inner pipes in S2	Inner pipe in S3
250	130	50	10

For this purpose, oxygen is fully discharged from all the sections and hydrogen is passed at a relatively great flow rate. When the heating is continued over about 10 minutes, the tapered portion is partially molten, followed by instantaneously pressing against the dummy rod and bonding together. The movement at the pressing is, for example, at about 60 mm. Thereafter, the flame is turned down, under which the bonded portion is parched for about 5 minutes. The flow rates for this purpose are indicated below.

Table 2

Flow rate of hydrogen (SLM)	Flow rate of oxygen		
	Group in S1	Group in S2	Group in S3
250	65	25	5

The bonding procedure set out above is for the preform having a diameter of 60 mm $\phi$ . If the diameter is increased to 80 mm $\phi$ , the flow rate has to be doubled with similar results.

It will be noted that although the bonding of a dummy rod at one end is depicted in Fig. 5A, the rods are usually bonded to opposite ends of the preform.

Fig. 5b shows elongation of a preform including heating and elongating steps where the tailstock is moved in a direction opposite to the case of Fig. 5a and the burner is also moved in the same direction as shown. In this case, high heating power as in Table 1 is necessary and the burner is turned up substantially in the same manner as in Fig. 5A. For the elongation, a preform having an uneven surface and a diameter, for example,



67 mm $\phi$  is elongated to obtain a flat surface-bearing preform having a diameter of 60 mm $\phi$ . When the flow rates of oxygen are determined, the tailstock and the burner are automatically moved at a given speed and a given movement according to signals from the control unit C. This  
5 automatic movement may be carried out in a stepwise manner or continuously in this and other cases.

Fig. 5C shows flame polishing on the outer surface of a preform. In Fig. 5C, the burner is moved while stopping the tailstock. This flame polishing is carried out to remove silica clouds from the preform surface, fine  
10 defects formed in the course of the manufacture of the preform and also a thermal strain from the inside of the preform. For the flame polishing, if heating power is too high, the silica deposited on the preform surface undergoes sublimation and may be, in most cases, re-deposited as a silica  
cloud on the preform surface. On the other hand, if the heating temperature  
15 is too low, the removal of defects and silica clouds may become unsatisfactory, or satisfactory heating to the inside of the preform is not possible with a residual strain being left. If the residual strain inside the preform is not removed to a satisfactory extent, cracks may be caused to occur in the vicinity  
of the preform surface on way of cooling after completion of flame polishing.

20 In the flame polishing, the intensity of heating power is an important parameter, not to mention the moving speed of the burner. Accordingly, the flow rates of gases and the moving speed of the burner should be optimized, as parameters, according to the outer diameter of the preform. More particularly, the flow rates of gases, the moving speed and  
25 the outer diameter of perform are interdependent.

With drawing as shown in Fig. 5D, initial heating is carried out under high heating power. At the stage where the preform is elongated to

an extent as to permit the preform just before melting up into pieces, whereupon the flow rates of a flammable gas and a supporting gas and the section or sections where the supporting gas is passed are properly selected or determined. Under these conditions, the thickness of the flame is  
5 gradually reduced, under which the tailstock is further moved to create an intended drawn shape.

In usual practice, the drawing may include primary heating, primary drawing, secondary heating and secondary drawing. The amounts of gases, movements and/or moving speeds of the burner and tailstock are, respectively,  
10 determined to obtain optimum flame conditions suited for the respective steps. These parameters are interrelated with one another and are not always critical, respectively. In order to cope with possible problems which may be involved in wide ranges of processings, it is necessary to permit the burner arrangement or system to be precisely controlled with respect to the  
15 heating power from the burner since the movements of the burner and the tailstock can be controlled as desired

In the drawing procedure, it is important to determine that a supporting gas be passed to whichever section or sections depending on the heating power conditions required for an intended step. More particularly,  
20 when the heating powder from the flame is turned down by reducing an amount of the gas while keeping the sections through which a supporting gas is flown, the preform is heated over a wide area thereof, unfavorably resulting in a drawn portion being elongated. To control the length of the drawn portion as desired requires a change in thickness of the flame per se  
25 by changing the section or sections through which the gas is flown or stopping a gas flow to the inner pipes in a certain section or sections. This is particularly described in example appearing hereinafter.

As described hereinabove, the flame thickness, and the flow rate of a flammable gas and the flow rates of a supporting gas through the sections can be controlled as desired, with the selection of whichever section or sections for the supporting gas being readily determined. The term  
5 “flame-controlled conditions” used herein is intended to mean those conditions established under these controls and the determination in relation to the movements and moving speeds of a tailstock and a burner unit.

Fig. 5E shows flame cutting after the drawing procedure, in which a thin flame is blown against the deeply drawn portion of the preform and  
10 cutting the preform by melting up into two pieces. The flame required for this purpose is one which is narrowed down and has a relatively high flow rate. For this purpose, flow rates of hydrogen used as a flammable gas and oxygen supplied to inner pipes at S1, S2 and S3 are as shown in Table 3 below.

15 Table 3

Flow rate of hydrogen (SLM)	Flow rate of oxygen		
	Group in S1	Group in S2	Group in S3
20	0	0	10

This processing may be replaced by flame cutting with a separately provided hand burner. The use of one burner for carrying out all the processing steps for preform according to the invention is very advantageous  
20 from the standpoint of labor saving and ease in automatic control of the processing parameters for preform.

As stated hereinabove, according to the invention, preforms having different sizes over a wide range may be processing into desired forms for substantially all preform processing procedures using one apparatus  
25 comprising a burner arrangement of a specific type while controlling processing conditions or parameters as desired.

The present invention is more particularly described by way of example, which should not be construed as limiting the invention thereto.

#### Example

A burner of the type shown in Fig. 2 was set in a glass-working lathe shown in Fig. 1 and was used to drawing of a preform having a size of 60 mm $\phi$ . This burner had an outer hollow cylinder made of SUS 304 and having an inner diameter of 30 mm $\phi$  through which a hydrogen gas was passed. In the outer cylinder, fine pipes made of SUS 304 and each having an outer diameter of 3 mm $\phi$  and an inner diameter of 1.5 mm $\phi$  through which an oxygen gas was passed were arranged concentrically while grouping the fine pipes into three from inside toward outside. The groups of the fine pipes in the respective sections were, respectively, connected to different oxygen gas feed pipes. Thus, one hydrogen gas feed pipe and three oxygen gas feed pipes were provided wherein each feed pipe had a manual valve and MFC connected in series. By controlling the respective MFC's based on signals from a control unit, the movements of the burner and a tailstock and also the amounts of the gases from the respective feed pipes could be set, followed by automatic operation of the lathe. The flow rate of a hydrogen gas to be supplied to the burner was at 500 SLM (standard liter per minute) in maximum, and the flow rates of three oxygen gas flows were, respectively, 250 SLM, 150 SLM and 10 SLM, each in maximum, in the order of from the outer peripheral side of the outer cylinder, i.e. from S1 to S3 in Fig. 3A.

The drawing procedure can be broadly divided, as set out hereinbefore, into four steps of primary heating, primary drawing, secondary heating and secondary drawing. In the respective steps, the amounts of the gases, and the movements and moving directions of the burner and the tailstock were set appropriately. In this example, these parameters were set

as shown in Table 4 below.

As a result, the length of the drawn portion (see Fig. 6) could be made as short as 62 mm, which was substantially the same as the diameter of the preform.

5                      Table 4

Steps	Amounts of gases from burners (SLM)				Movement of burner (mm)	Movement of tailstock (mm)
	Hydrogen	Oxygen (S1)	Oxygen (S2)	Oxygen (S3)		
Primary heating	250	130	50	10	0	0
Primary drawing	200	110	40	10	5	10
Secondary Heating	130	0	60	7	5	10
Secondary drawing	100	0	50	5	20	30

#### Comparative Example

Four burners of the type shown in Fig. 7 were attached to a glass-working lathe shown in Fig. 1 so as to process a preform having a size of 60 mm $\phi$ . This burner was of the type wherein hydrogen gas was blown out from a peripheral portion thereof and oxygen gas was blown out from an inner portion. Both gases were mixed at the tip of the burner and combusted. Like Example 1, the gas feeds to the burners were, respectively, changed in the order of the primary heating, primary drawing, secondary heating and secondary drawings, the burners and the tailstock were moved to form a drawn portion.

The gas feeds to the respective burners were so designed to be at 100 SLM in maximum for hydrogen gas and 50 SLM in maximum for oxygen gas, and the flow rates of the gases simultaneously supplied to the respective burners were equal to one another. The intensity of the resulting flame was controlled by simultaneously changing the gas feeds to all the burners. The

gas feed per unit burner is shown in the table shown below, and a total gas feed is as much as four times the gas feed indicated below.

Table 5

Steps	Gas feed to burner (SLM)		Movement of burner (mm)	Movement of tailstock
	Hydrogen	Oxygen		
Primary heating	80	40	0	0
Primary drawing	60	30	5	10
Secondary heating	20	10	5	10
Secondary drawing	15	7	20	30

5                    When the preform was drawn under conditions indicated in Table 5 above, the flame extended over a length of the preform, especially after the secondary heating, irrespective of the fact that the gas feed passed to the burners was reduced. As a result, the portion of the preform whose diameter was reduced was entirely heated, thus resulting in the drawn portion being  
10 elongated to 120 mm.

                    Thus, according to the invention, the thickness and intensity of a flame can be appropriately controlled depending on the manner and conditions of processing of a preform, thereby creating flame-controlled conditions satisfactory for different processing procedures of a preform. The  
15 thickness or shape and intensity of a flame can be appropriately controlled while taking the diameter of a preform into consideration. A preform can be processed into a desired form using the same apparatus only by changing preset conditions.

20